# **TANK SAFETY & PROTECTION DEVICES**

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31 October - 3 November 2022 Abu Dhabi, United Arab Emirates



Korea Steel Power Corp.





## K.S.P.C **VISION & MOTTO**

VISION Safety is the first and most important. Think about Environment

Truly think and consider customers. Truly make eco-friendly safe world safe world products.

## QUICK ACCESS TO ITEM CATALOGS IN QR CODES

PRESSURE VACUUM RELIEF VALVE



EMERGENCY RELIEF VALVE



GAUGE HATCH COVER .....

NITROGEN BLANKETING VALVE



Quick access to KSPC website in QR code



Quick access to valve operating video in OR code





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# PRESSURE VACUUM RELIEF VALVE



Pressure Vacuum Relief Valve is designed to protect low pressure storage tanks from excessive pressure or vacuum created by thermal expansion (and contraction) and product movement into(out of) the tank and at the same time minimizing costly product evaporation/loss.

SETTING PRESSURE	WEIGHT LOADED MODEL ±20 mmW.C ~ +700/-430 mmW.C		
SETTING TRESSORE	SPRING LOADED MODEL	+700/-430 mmW.C~ ±9,000 mmW.C	
SIZE RANGE	DN 50 ~ DN 350 with ASME 150# flanges (different connections available on request)		
BODY MATERIAL  Aluminum, Carbon Steel, 304 Stainless Steel and 316 Stainless Steel with various trims (different materials available on request)			
RULES & CERT.	API 2000, ATEX		

04 |



## **VALVE OPERATION** & SIZING CALCULATION &

### A. VAI VF OPERATION

According to API 2000 code, the Pressure vacuum relief valve are designed, manufactured and tested. The Pressure Vacuum Relief Valves are used on liquid storage Tanks which designed by API 520/API 650 and Others process vessels or systems to prevent structural damage due to excess internal pressure or

This valve has functions to intake the air under constant pressure during unloading and rising Temperature, and to discharge the overpressure generated during pouring the liquid and falling Temperature on storage tank. This is the safe valve to control the deflation(vacuum) and inflation(pressure) of several storage tanks.



The function of prevention of natural evaporation of fluids

#### THE EFFECT OF ENERGY REDUCTION In

case of gasoline, to minimize the natural evaporation of stores saves 98m3 per year. (Based on the tank diameter: 30.4m x tank capacity 8690m)

THE EFFECT OF PREVENTION OF

**EXPLORATION** With the exception of

influx and efflux of stores, it is Kept



of over-pressure

always closed to prevent the diffusion of exploration into tank.



The function of protection of under pressure

THE EFFECT OF PREVENTION OF CORROSION (The effect of extension of life). To keep the stabilization of constant gas pressure generated pressure generated inside tank, prevents inside of the tank from corrosion by the temperature of gas.

#### WHEN TANK IS UNLOADING PHENOMENA AND THE

RESSURE is above the setting(operational fixing pressure), the Pressure Vacuum Relief Valves operates automatically to protect the storage tank from the deflation or malformation.

The weight loaded type models are designed to provide tank protections for both pressure and/or vacuum of set point to max 75/-43 mbarg.

Over 75/-43 mbarg set point till 900/-900 mbarg, consider to be installed spring loaded type. Safety relief valve is not used in controlling the extra setting of pressure and consider Emergency vent for External fire and Rupture case.

The set point of Pressure vacuum relief valve is fixed by the customer's order or Project's Specification. but it is designed to adjust the pressure / vacuum setting in case. The way of change adds additional counter weight for Weight loaded type. The way of change for spring loaded as follow.

To increase the setting pressure turns the press, adjusting screw clockwise. To decrease the setting pressure turns the press. adjusting screw counter-dockwise. Before change set point of disc A'ssy, should be consulting the factory or our local representative.





Unloading condition

#### B VALVE SIZING CALCULATION

 Required Inbreathing and Out-breathing capacity for your applications should be determined by using API2000 standard.

**B-1** Total Out-breathing caused by liquid movement and vaporization - Liquid movement (section 3.3.2.2.1 in API 2000 7th)

$$\dot{V}_{op} = \dot{V}_{pf}$$

: Out-breathing volumetric flow rate (Nm3/h of air) at the actual pressure and temperature conditions of the tank vapor space with a vapour pressure equal to or less than 5.0 kPa.

V<sub>20 f</sub>: Maximum volumetric filling rate (Nm³/h) of nonvolatile liquids.

$$\dot{V}_{op} = 2.0 \cdot \dot{V}_{pf}$$

: Out-breathing volumetric flow rate (Nm3/h of air) at the actual pressure and temperature conditions of the tank vapor space with a vapour pressure greater than 5.0 kPa.

 $V_{pf}$ : Maximum volumetric filling rate (Nm³/h) of volatile liquids.

#### - Thermal effect (section 3.3.2.3.2 in API 2000 7th)

$$V_{OT} = Y \cdot V_{tk}^{0.9} \cdot R_i$$

V: is a factor for the latitude

(search for the number in the table. Refer API2000 3.3.2.3.2)

Latitude	Y-factor
Below 42°	0.32
Between 42° and 58°	0.25
Above 58°	0.2

 $V_{eb}$ : is the tank volume. (m<sup>3</sup>)

R: is the reduction factor for insulation.

$$R_{inp} = \frac{A_{inp}}{A_{rts}} \cdot R_{in} + \left(1 - \frac{A_{inp}}{A_{rts}}\right) \qquad R_{in} \frac{1}{1 + \frac{h \cdot l_{in}}{\lambda}}$$

There are three cases in getting R

No. insulation: R=1

Fully insulated

- 1: The inside heat-transfer coefficient (W/m2-K)
- lin: the wall thickness of the insulation (m)
- \(\lambda\_{im}\): The thermal conductivity of the insulation (W/m<sup>-K</sup>)

#### 3) Partially insulated

- Arre: The total tank surface area (shell and roof) (m2) - A<sub>(mp)</sub>: The insulated surface area of the tank (m<sup>2</sup>)

B-2 Total In-breathing caused by liquid movement and vaporization - Liquid movement (section 3.3.2.2.1 in API 2000 7th)

$$V_{ip} = V_{pe}$$

: Out-breathing volumetric flow rate (Nm3/h of air) at the actual pressure and temperature conditions of the tank vapor space with a vapour pressure equal to or less than 5.0 kPa.

 $V_{ip}$  : Maximum volumetric filling rate (Nm³/h) of nonvolatile liquids.

-Thermal effect (section 3.3.2.3.2 in API 2000 7th)

$$\dot{V}_{it} = C \cdot V_{tk}^{0.7} \cdot R_i$$

: is a factor that depends on vapour pressure, average storage temperature and latitude.

	C-factor for various conditions				
	Vapour pressure				
Latitude	Average storage temperature, °C				
Loutage	Hexane or similar		Higher than hexane, or unknown		
	<25	≥25	<25	≥25	
Below 42°	4	6.5	6.5	6.5	
Between 42° and 58°	3	5	5	5	
Above 58°	2.5	4	4	4	

 $V_{+k}$ : is the tank volume. (m<sup>3</sup>)

 $R_i$ : is the reduction factor for insulation. The way to calculate  $R_i$  is equivalent to the method which is in the upper part of this page.

The size of the valve shall be selected by comparing our certified flow / pressure drop diagrams with calculated inbreathing and out breathing.

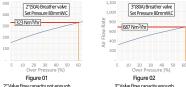
#### - Check point

1) Set pressure: The adjusted pressure or vacuum which valve start to open. Over pressure: Pressure increase at the valve inlet above the set pressure or vacuum. 3) Over pressure calculation

- Example.1
- Valve set pressure = 50mm,W.C
- Tank Design pressure = 80mmW.C
- Max. allowable over pressure = 60% (80mmW.C = 1.6times of 50mmW.C) -Example.2
- · Valve set vacuum = -50mm.W.C
- Tank Design vacuum = -100mmW.C
- Max. allowable over pressure = 100% (-100mmW.C = 2times of -50mmW.C)

4) Size select comparing flow/pressure drop diagram with calculated inbreathing and out breathing

- Example (Check figure 01 & 02)
- Calculated Out breathing = 500m<sup>3</sup>/hr
- Valve set pressure = 80mmW.C
- · Calculated Max. allowable over pressure = 60%



2" Value flow canacity not enough to meet calculated Out breathing 500Nm3/hr to meet calculated Out breathing 500Nm3/hr

5) According to API2000. The maximum overpressure shall be 2 times of adjusted set pressure or vacuum. If the fully open position of the valve disc is not achieve at two times the adjusted valve set pressure, one step above size or additional measuring point(=additional valve) are required until the fully open position is reached to calculated in/out breathing.

\* Note: Direct-acting vent valve are typically available in size from 50mm to 350mm.



Pressure /

vacuum relief w /

flame arrester



# **EXECUTE** VENT TO ATMOSPHERE PRESSURE VACUUM RELIEF VALVE

\* Vent to ATM pressure vacuum relief valves are an advanced design for vent to atmosphere applications.

Designed manufactured and tested according to the API2000 code. It is a safety device made in response to the pressure and vacuum in the storage tank. Opening at accurate settings, it protects the tank from damages due to explosion and vacuum, minimizes the loss of product by prevention leakage of the tank and protects environment from poisonous gases.



# PRESSURE VACUUM RELIEF VALVE

\* Pipe away pressure vacuum relief valves are an advanced design for pipe away application.

Designed manufactured and tested according to the API2000 code. It is a safety device made in response to the pressure and vacuum in the storage tank. Opening at accurate settings, it protects the tank from damages due to explosion and vacuum, minimizes the loss of product by preventiog leakage of the tank and protects environment from poisonous gases.



steam jacket

Pressure /

vacuum relief w /

flame arrester



Pressure /

vacuum relief w /

dehumidifier

Pilot operate valve



Vacuum relief

Vacuum relief (Spring loaded type)

w/Steam jacket



## **FLAME ARRESTER**

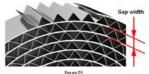


Flame Arrester is used for preventing flame transmission when an explosion is occurred inside of the piping which full of explosive mixed gas

OPERATING TEMPERATURE @ PRESSURE	+60 °C @ 0.11 Mpa
SIZE RANGE	DN 50 ~ DN 1000 with ASME 150# flanges (different connections available on request)
BODY MATERIAL	Aluminum, Carbon Steel, 304 Stainless Steel and 316 Stainless Steel with various trims (different materials available on request)
RULES & CERT.	ISO 16852, ATEX

## FLAME ARRESTER OPERATION & SELECTION &

Flame arresters are passive devices with no moving parts. Flame arresters prevent the propagation of flame from the exposed side of the unit to the protected side by the use of wound crimped metal ribbon type flame cell element(Figure 03). This construction produces a matrix of uniform openings that are carefully constructed to guench the flame by absorbing the heat of the flame. This provides an extinguishing barrier to the ignited vapour mixture. Under normal operating conditions the flame

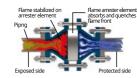


arrester permits a relatively free flow of gas or vapour through the piping system. If the mixture is ignited and the flame begins to travel back through the piping, the arrester will prohibit the flame from moving back to the gas source.

#### Flame arrester operation

When the combusted gas pass through the heat exchange lattace net of the element bank of the flame arrester in inline Flame arrester type, the combusted gas ignified by the guenching is completely extinguished by lowering the temperature under below the natural ignition point. Thus, this item is designed to extinguish the fire automatically, and the heat is absorbed by the element bank of flame arrester and the fire cannot be spread.

#### MESG (Maximum Experimental Safe Gap)



Measurement of the maximum gap between two equatorial flanges on a metal sphere that will prevent a flame from being transmitted from the sphere to the surrounding flammable mixture. MESG is dependent on gas composition.

Range of application (marking)		R	equirments f	or test mixtur	e	
	Explosion group	MESG of mixture mm	Gastype	Gas purity by volume %	Gas in air by volume² %	Safe gap of gas-a mixture mm
	IIA1	≥1,14	Methane	≥98	8,4±0,2	1,16±0,0
	∐Ab	>0,90	Propane	≥95	4,2±0,2	0,94±0,0
	IIB1b	≥0,85			5,2±0,2	$0.83 \pm 0.0$
	IIB2b	≥0,75	Ethylene	≥98	5,7±0,2	$0,73 \pm 0,0$
	IIB3>	≥0,65			6,6±0,3	$0,67 \pm 0,0$
	IIB1⁵	≥0,50	Hydrogen	≥99	45,0 ± 0,6	1,16±0,0
	IIC	<0,50	Hydrogen	≥99	28,5 ± 2,0	1,16±0,0

Flame arrester selection

Flame propagation poses significant dangers to systems and personnel in industries worldwide. Careful consideration must be taken to determine whether to use a Flame Arrester or a Detonation Flame Arrester. There are two basic determinations when evaluating the intended application:

O. The location of the ignition source from the flame

O. What needs to be protected.

First, determine the location of all potential ignition sources (i.e. flare, vacuum pump, blower, burner, lightning strike, static discharge, etc).

Second, evaluate the system to determine exactly what should be protected (i.e., the gas source, process component, personnel, upstream process facility, tank, etc.).

When you have determined the ignition source(s) and what is to be protected, the following parameters should be evaluated in order to determine the appropriate flame arrestment protective device:

1. Length and configuration of pipe and pipe between ignition source and arrester.

2. System gas grouping. 3. Initial operating pressure. 4. Flame stabilisation on element.

All of these variables affect the performance of the arrester and can also affect the dynamics of flame propagation

#### Inline and End of Line Applications

The inline flame arrester and the end of line (free vent) arrester are used to stop flame propagation of confined and unconfined low pressure deflagrations. They are typically used for limited piping applications when the system operating pressure is near atmospheric levels.

#### Detonation application

The detonation flame arrester is an advanced technology flame arrester. They are used to stop the high pressures and velocities associated with detonation. They stop confined and unconfined low and high pressure deflagrations, stable and overdriven detonations. Application parameters for the detonation flame arresters far exceed those of flame arresters for pipe lengths, configurations, system operating pressures, and flame stabilization. Our flame arresters are designed, manufactured and tested according to BS7244. BSEN12874 and ISO16852 test standards and codes.

#### System gas grouping

The type of gas in the system and it's corresponding gas group determines the design of the arrester element. The SS316L element must be designed to accommodate the specific gas group that could possibly ignite and propagate in the system. The available designs consist of International Electric Code (IEC) group gases into IIB,IIA and IIC, the National Electric Code (NEC) groups gases into A, B, C and D categories depending on the MESG value of the gas.

#### GAS GROUP CHART

### Group A Acetlyene

Butadiene Ethylene oxide

Acetaldhyde Diethyl ether

The stoichiometric mixture is used to determine the minimum MESG value for a given gas.

Hydrogen Manufactured gases containing (by volume) ropylene oxide

Dimethylhydrazine Ethylene Hydrogen sulfide \*Methanol (methyl alcohol) Methyl mercoptan

Acrylonitrile Butylene 1-Butanol (butyl alcoholl 2-Butand (secondary butyl dcohol Cyclohexane N Butyle ocetate sobutyl gcetate Ethone.echoll Ethanol (ethyl alcohol) Ethyl acetate. Ethyl acrylate Ethylene dichloride Gasoline Heptanes Hexanes soprene Methane (natural gas Methyl acrylate Methylamine Methyl ethyl ketone

isoamyl alcobbol) Methyl isobutylketone 2-Methyl-1 propanol isobutyl clcohol) Methyl-2-propanol tertiary butyl alcohol Naphtha (petroleum) N Propyl acetate Octanes Pentanes 1-Pentanol (amyl aloohol) Propane 1-Propanol (propyl alcohol 2-Propanol (isopropylalcoho Propylene Styrene Toluene Turpentine Vinylacetafe Vinyl chloride





# **EX** DEFLAGRATION FLAME ARRESTERS

Deflagation flame arresters provide positive protection against flame propagatin to the protected side in case of deflagration of explosive vapor/air or gas/air mixtures.

They are designed to protect against continuous burning against the 316LSS flame cell elements for a specific period.



KSFI / KSFI-A TYPE

Inline flame arrester
Possible to install vertically and horizontally



KSFIJ type

Flame arrester w / steam jacket



KSFH type

Inline flame arrester
Possible to install vertically and horizontally



KSFE / KSFE-A type

End line flame arrester Should be installed vertically



KSFE-J type

Flame arrester w/ steam jacket



KSFE-S type

End line flame arrester, Should be installed vertically



KSFL type

Inline flame arrester Should be installed horizontally



KSFT type

Inline flame trap



KSFF type

Deflagration proof end-line flame arrester



# © DETONATION FLAME ARRESTERS

Detonation flame arresters provide positive protection against flame propagation in piping systems that are manifolded or have long runs.

The arresters are designed to stop and ignited flammable vapour mixture travelling at subsonic or supersonic velocities

They are also designed to protect against continuous burning against the 316LSS flame cell elements for a specific period



KSFD-A type

Inline detonation flame arrester, Possible to install vertically and horizontally



KFD type

Inline flame arrester
Possible to install vertically
and horizontally



KSFLD type

Inline flame arrester Should be installed horizontally



KSFM type

Inline flame arrester Should be installed right angle pipe line



KSFD type

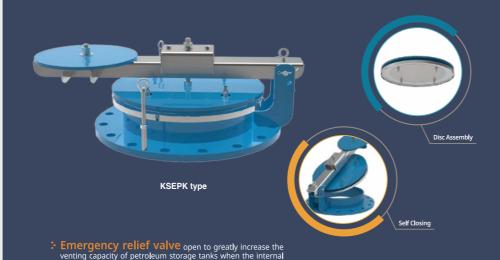
Inline flame arrester Should be installed horizontally



# EMERGENCY RELIEF VALVE

pressure rises above the set point. it remains closed tightly when

internal pressure below the settings.



SETTING PRESSURE	WEIGHT LOADED MODEL	+50 /-25 mmW.C ~ ±700 mmW.C
SETTING TRESSORE	SPRING LOADED MODEL	+700/-20 mmW.C ~ ±9,500/-700 mmW.C
SIZE RANGE	DN 400 ~ DN 750 with ASME 150# or API 650 flanges (different connections available on request)	
BODY MATERIAL	Aluminum, Carbon Steel, 304 Stainless Steel and 316 Stainless Steel with various trims (different materials available on request)	
RULES & CERT.	API 2000, ATEX	

# VALVE OPERATION & SIZING CALCULATION &

#### A. Valve operation

Emergency relief valve is the safety valve to protect the storage tank from the inflation/pressure) with the function to discharge rapidly the overpressure developed during external fire around the storage tank or the Excessive fluid intake more than the capacity of purmo planned.

Emergency relief valve is designed to be Cushioned air seating, Teflon (PTFE/FEP-2 Layer) seating diaphrapm are Standard. It minimize sticking caused by resinous vapors and atmospheric moisture. The Seat tightness is 75% of set point by API 2000. It is designed to be self dosing under normal operation by Internal Guide & external Hinge and the restraining cable to Connect the Cover assembly and Flanges also serve a grounding cable.



The Emergency relef valve provides pressure / or vacuum relief when the tank is bading phenomena and external fire or Rupture cases also the pressure is above the setting (Operational Fixing pressure), the Emergency relief valve operate automatically to protect the storage tank from inflation.

The weight loaded type model max. set point is 70/-43mbarg and spring loaded type is till 900/-900 mbarg.

#### B. Valve Sizing

Where the fluid properties are similar to those of hexane, the required venting capacity

If the height of the tank exceeds 9.14 meters, use the same number to the tank which is higher than 9.14 meters for calculation. If wetted surface area is wider than 260 m², there are two cases. Refer to the following table 01.

Wetted surface area	Design pressure kPa (gauge)	Required Venting Calculation Nm³/h of air
<260	≤103.4	See table 03
≥260	≤7	19910
≥260	>7 and ≤103.4	$q = 2082 \cdot F \cdot A_{\text{max}}^{-0.82}$

Table 0

$$A_{TWS} = \pi \cdot D \cdot L$$
  $A_{TWS} = \pi \cdot D \cdot L \cdot 9.14$ 

(In case of L<9.14 meters)

(In case of L>9.14 meters)

Where the fluid properties are other than hexane, the required venting capacity can be calculated given by below equation.

$$q = 906.6 \cdot \frac{Q \cdot F}{L} \cdot \left(\frac{T}{M}\right)^{0.5}$$

q is the heat input from fire exposure as given by Table 02, expressed in watts. F is the environmental factor from table 09(API2000 Clause 3.3.3.3.2). L is the latent heat of vaporization of the stored liquid at the relieving pressure and

temperature, expressed in joules per kilogram.

T is the absolute temperature of the relieving vapor, expressed in kelvins

Mis the relative molecular mass of the vapor

Wetted surface area	Design pressure kPa (gauge)	Heat Input,Q W
<18.6	≤103.4	63,150 A TWS
≥18.6 and <93	≤103.4	224,200* (A TW3 0.566)
≥93 and <260	≤103.4	630,400*(A+1113 <sup>0,388</sup> )
≥260	>7 and ≤103.4	43,200*(A7W3 <sup>0.82</sup> )
>260	<7	4.129.700

Table 02

Wetted area <sup>a</sup> (Square meters)	Venting Requirment (Nm <sup>3</sup> /h)	Wetted area <sup>a</sup> (Square meters)	Venting Requirement (Nm³/h)
2	608	35	8086
3	913	40	8721
4	1,217	45	9322
5	1,521	50	9895
6	1,825	60	10,971
7	2,130	70	11,971
8	2,434	80	12,911
9	2,738	90	13,801
11	3,347	110	15,461
13	3,955	130	15,751
15	4,563	150	16,532
17	5,172	175	17,416
19	5,780	200	18,220
22	6,217	230	19,102
25	6,684	260	19,910
30	7,411	>260 <sup>b</sup>	-

Table 03

The size of the valve shall be selected by comparing our certified flow / pressure drop diagrams with calculated inbreathing and out breathing.

#### Check point

Set pressure: The adjusted pressure or vacuum which valve start to open.
 Over pressure: Pressure increase at the valve inlet above the set pressure or vacuum.
 Overpressure calculation

#### Example

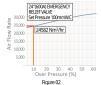
-Valve set pressure = 100mm.W.C(90% or same as tank design pressure)

- -Tank Design pressure = 100mmW.C
- Max. allowable over pressure = 10%(Emergency relief valve set pressure is usually 90% or same as Tank design pressure hence max. allowable design pressure is 10% generally Size select comparing flow/pressure drop diagram with calculated emergency out breathing.
- Example (Check figure 01 & 02)

  · Calculated Out breathing = 19,910m<sup>3</sup>/hr
- · Valve set pressure = 100mmW.C
- · Calculated Max. allowable over pressure = 10%



20" Valve flow capacity not enough to meet calculated Out breathing 19,910Nm<sup>3</sup>/hr

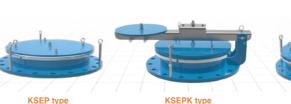


24" Valve flow capacity enough to meet calculated Out breathing 19,910Nm³/hr





## **EX WEIGHT LOADED TYPE**



KSEP type

Pressure relief

Pressure relief Hinged type

- closed automatically

KSEV type

Pressure / vacuum relief



KSEVK type

Pressure / vacuum relief Hinged type - closed automatically



KSEVJ type

Pressure / vacuum relief w / steam iacket



KSEPW type

Pressure relief Water seal type - zero leakage at set point

## SPRING LOADED TYPE



KSES type Pressure relief



Pressure / vacuum relief

## **NITROGEN BLANKETING VALVE**



DST100/200 type

\* Nitrogen Blanketing Valve helps gas pressure to maintain In constant state in the vapour space of storage tanks.

When liquid run out from storage tanks or vacuum state take place because of temperature dripping, N2 blanketing Valve has a ability of control desired pressure within the fixed limits.

Besides about subjects, prevents air and humidity from entering into storage tank, so it can preserve product, and also protect from a fire.

It protects the tank from explosion by restriction spark. It prevents the outflow of fluid by evaporation.



SIZE		DST-100		DST-	200
SIZE	1/2"	3/4"	1"	1½"	2"
N.D	15	20	25	40	50
Α	290	290	290	340	340
Approx. H	355	355	355	415	415

NOTE Standard Connection (ANSI 150LB flange) and JIS or different types are available upon request.

OLIVLIAL SI ECII ICATION			
MODEL	DST-100	DST-200	
SIZE	1/2" ~ 1"	1"~ 2"	
SET PRESSURE	30 ~ 5000mmW.C		
CONNECTION	FNPT / ANSI 150# & 300#, Etc		
MATERIAL	SS304, SS316, Etc.		
USED GAS	N2 (Nitrogen)		
SENSING PORT	NPT½"		

SET PRESSURE		MINIMUM INLET PRESSURE	ТЕМР.
1.2 ~ 1.4" W.C	1.3 ~ 3.1 psi	22 psi (1.5 kg/cm <sup>2</sup> G)	-20 to +149 °C
3.5 ~ 10" W.C	2.3 ~ 3.5 psi		
8 ~ 18" W.C	3.0 ~ 6.0 psi		



# & SLOT DIPPING DEVICES



KSGE type

Operating pressure - 0.01 kg/arr



KSGH type

Operating press - 0.03 kg/om²

KSPC's Sampling and Gauging Hatch Cover is designed to provide quick access for product gauging, temperature measurement or sampling.

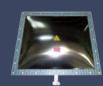


\* KSSD Series Sampling Device is designed for gauging the height of liquid levels, measuring the depth of water bottoms, and taking sample of liquids held in storage tank, without relieving pressure within the tank.



## **RUPTURE DISC**





Rupture Disc holder and disc assembly

Rupture Disc

Explosion Panel

A Rupture Disc is a non-mechanical safety device to relief when it is occurred that excessive pressure is over the critical pressure in a pressure system

#### When is it required a Rupture Disc?

- $\cdot$  In case of a rapid rise in pressure as a result of runaway reaction and so on
- In case that there is any concern that fixtures cause other safety device malfunction
- · In case that any leakage is not permitted
- · In case that it contains strong corrosive fluid
- In case that it requires large relieving capacity in an instant by polymerization and so on
- · Severe conditions such as high or low temperature

#### Features

- · Special material and structure (It is easy to select material and is economical) And there is no size limit
- · Constant rupture performance and release all of fluid
- · Instantaneous release of maximum capacity
- · Extensive service environment
- (strong corrosive fluid, temperature, liquid, gas, powder, etc.)
- · Zero Leakage
- · Extension of safety valve life
- · Possible to check the Piping of outlet during operating
- Extension of overhaul period
- · Easy to handle and cost reduction

#### Applicable Code

- · ASME Sec. VIII Div.1
- · ISO 6718
- · ISO 4126-2~6
- · API RP520
- · KOSHA Safety Certification

#### When is it required a Rupture Disc

- · Stainless Steel (304SS, 316SS, 317SS, etc)
- · Carbon Steel · Duplex
- · Aluminum
- · Nickel, Inconel, Monel, Hastelloy, Titanium, Tantalium
- · Graphite
- Tofloo
- · Maximum usable Temperature

Teflon	200 ℃	Monel	483 ℃
Aluminum	120 °C	Inconel	592 ℃
Stainless Steel	483 ℃	Hastelloy	483 ℃
Nickel	403 ℃	Graphite	371 °C

#### Application of Rupture Disc

1) Primary Case 2) Secondary Case



3) Combination Case



4) External Fire Case





18 |







\* Air release valve is designed to release accumulated air pockets from the system, while pressured pipelines. Air pockets increase energy consumption because pumping operation will be at higher water heads to overcome pressured air. Air release valves are have function to protect high shock and surge pressure, water hammer and liquid overflow from fresh or sea water pipelines.

# Application

#### Operation Principle





PRESSURE / VACUUM RELIEF

## **Quality & Environment Certification**



ISO 9001



ISO 14001

## Type Approval Certification



KFI ATEX

20 |

#### Tank Protection Devices

- · Flame Arrester
- · Breather Valves
- · Air Release Valve
- · Vacuum Breaker
- · Pilot Operating Pressure / Vacuum Valves
- · Emergency Relief Valve
- · Gauge Hatches

- · Sampling Dipping Devices
- · Flame Trap Assembly
- · Floating Suction
- · Roof Drain System
- · Oil Skimmer
- · N2 Blanketing
- · Rupture Disc

#### : Application Fields

- · Offshore & Ocean Gas Plants
- · Marine Tank Ships
- · Cryogenic Gas Facilities
- · Sea & Fresh Water Plant
- · Tank Terminals
- · Refinery Tank Farm
- · Gas Plants
- · Oil & Chemical Storage Tanks









# 1

# company Information

KSPC at a Glance
Company History
Organization

# **KSPC** at a Glance



## **Established**

1991.3.1



## capital

\$ 200,000



## sales in 2019

\$10,000,000



## **Employees**



## **World-wide Networks**

**31 countries** 



## Factory & Head Office

Busan, Kimhae, Gimpo



## Plant / Factory Area

7,500 / 3,400 m<sup>2</sup>



## **Brach Offices**

Kimhae, Ulsan, Yeochon 📀

# **Company History**

1991 Established KSPC at Hanam City, Kyoung-Ki Province

1994 Moved HQ & built new factory at Kimhae City, Kyoung-Nam Province

1996 Established a Research Institute of Technology

1998 Obtained ISO9001 Certificate

1999 Awarded The first Kyoung-Nam Best Trader by Kyoung-Nam Province

2010 Moved office & built new factory at Gimpo City named to Korea Steel Power Corp.

1900

2010

## 2000

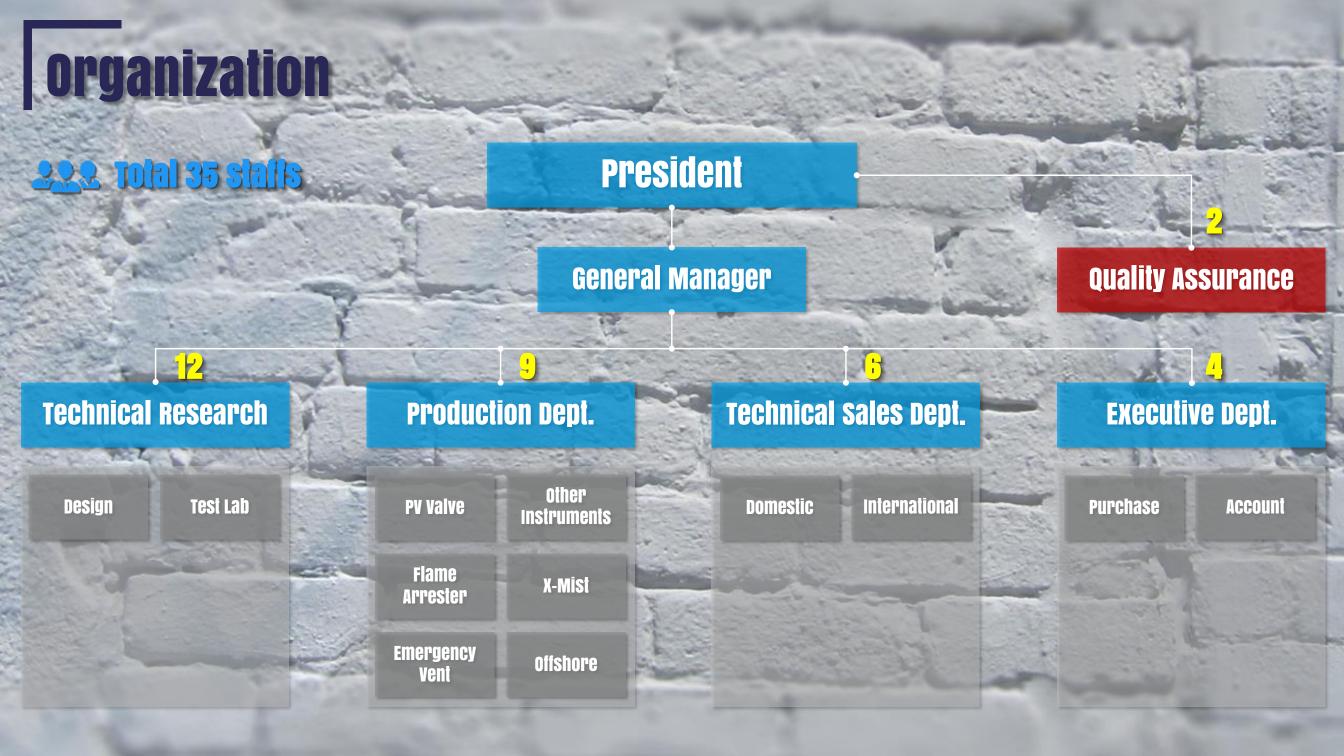
2000 Established company name to TANKTECH CO LTD

2001 Obtained USCG Certification for NEW-ISO-HV SERIES

2002 Won Official Commendation from Minister of Ministry of Commerce

2003 Developed Water Mist Firefighting System (X-MIST) & Tank Cleaning

Machine (PM-80)



# 2 Main Products

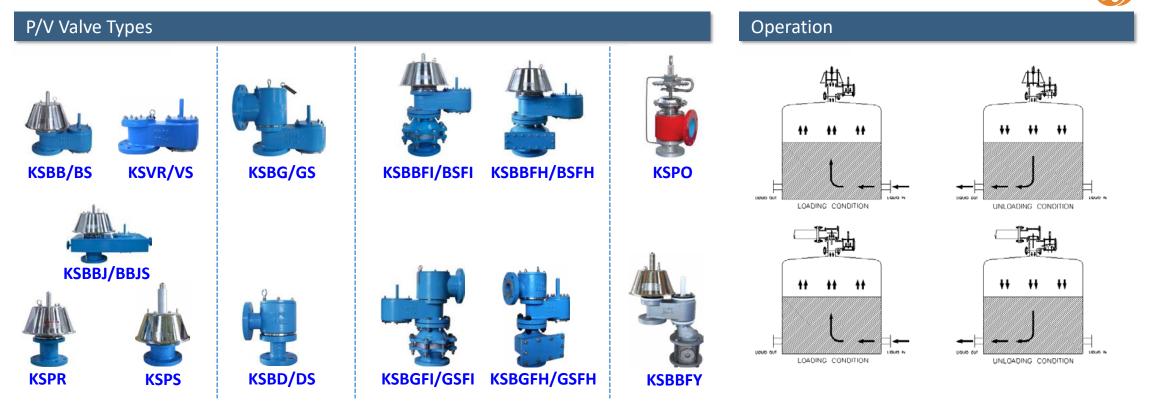
safety & Protection System **Automatic Tank Cleaning System** Fire Fighting System



## Pressure Vacuum Relief Valve

**KSPC Pressure Vacuum Relief Valves** are designed manufactured and tested according to the API 2000 code, these valves utilize the latest technologies to provide protection against positive or vacuum over pressure and prevent air intake, evaporative losses of product and help to contain odorous and potentially explosive vapor.



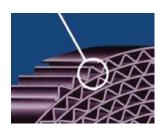


## Flame Arrester



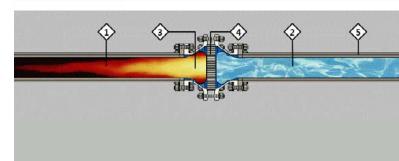


KSPC Flame Arrester of the model KSFI/FH is designed, manufactured, and tested according to ISO 16852 / EN12874 code. Installed in the top nozzle of the several kinds of the flammable low pressure storage tank (the ignition point below 65°C), it is the explosion proof and deflagration proof which blocks the influx of flame ignified externally into the tank.





### Operation



- 1 Exposed Side
- 2 Protected Side
- **3** Flame Stabilized on arrester element
- **4** Flame arrester element absorbs
- **5** Piping

## **Emergency Vent Cover**



**KSPC Emergency Vent Covers** provide the capacity to meet API standard 2000 for emergency venting due to fire exposure when properly sized. These covers also provide quick easy access for tank inspection and maintenance.

The KSEP/EPK emergency pressure relief vent provides pressure relief only.

Vacuum relief must be supplied by normal venting devices, or use our KSEV emergency pressure and vacuum relief vent covers. When excessive pressure builds within the storage tank the KSEP series emergency pressure relief vent begin to open at a predetermined set pressure relieving excessive pressure. And when the overpressure has dissipated the cover reseat onto the base.

### **Emergency Vent Cover Types**



**KSEP** 



**KSEPK** 



**KSES** 



**KSEV** 



**KSEVK** 



**KSESV** 

# Gauge Hatch, N2 Blanking, R/Disc







GH

SD









## N2 Blanking System



## Rupture Disc



## **Explosion Panel**





## Gauge Hatch with Tank Measuring

**Portable Oil/Water Interface Detector**, T2000 series offer total solution for management of cargo in tanks. This device can detect and measure the Ullage, Oil/Water Interface and Temperature Gauging of cargo at the same time.

- Measurement of tank liquid storage level, Water bound and Ullage
- Measurement of tank liquid temperature
- Inert Gas Sampling
- Liquid Sampling
- Inert Gas Pressure measurement
- Dryness check (hand Dipping)

## Portable Measuring Devices



T2000-TFC-01
Oil/Water/Ullage



Liquid Sampling

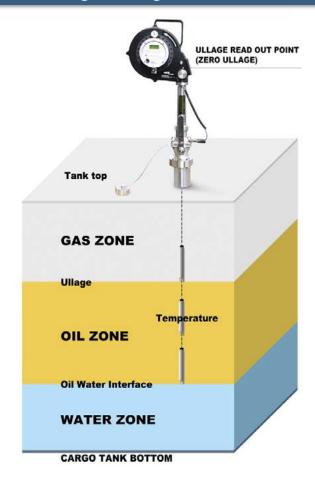
1

Inert Gas Pressure



**Dryness Check** 

### Tank Measuring on Gauge Hatch Cover



## Air Release Valve

**KSPC Air release valves** are designed to release accumulated air pockets from the system, while pressured pipelines. Air pockets increase energy consumption because pumping operation will be at higher water heads to overcome pressured air. Air release valves are have function to protect high shock and surge pressure, water hammer and liquid overflow from fresh or sea water pipelines.

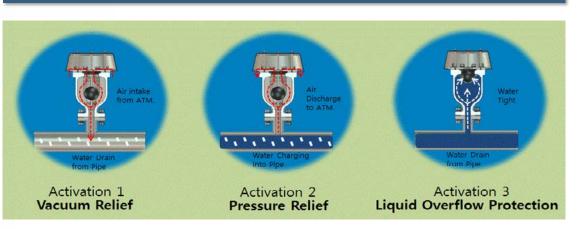
KSBJ air release valve can provide low cast insurance to protect expensive maintenance cost of pipelines and pump systems.

### Air Release Valve Function

- Anti-Surge & Anti-Shocks
- Surge and Water-hammer Protection
- Liquid Overflow Protection
- Release air pocket from pipeline
- Increasing of pump efficiency
- Less system energy
- Maintenance free



### Operation





# **Automatic Tank Cleaning Machine**



**Automatic Tank Cleaning System** is using fresh crude oil or cleaning chemical as cleaning agent. And the cleaning pump supplies the fresh crude oil to the tank cleaning machine through the flexible hoses.

## Application Procedure

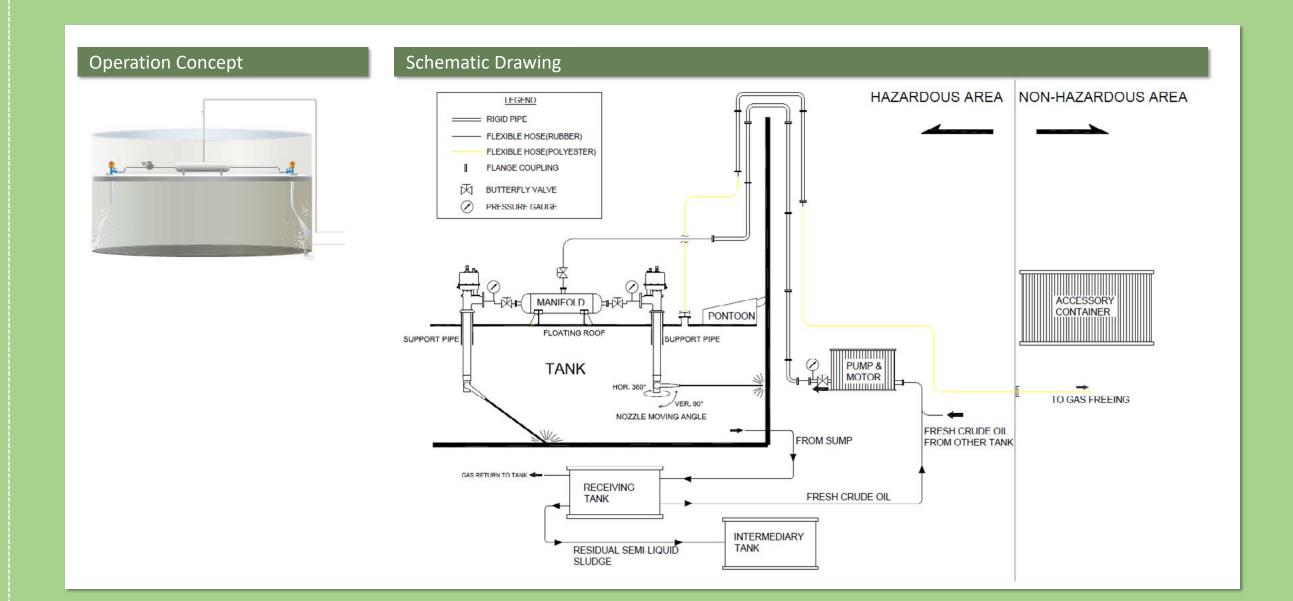
- **1** Measuring of sludge profile
- **2** Installation plan
- **3** Automatic tank cleaning
- **4** Extraction of sludge-oil mixture
- **5** Measuring of sludge profile
- **6** Repeat step 3 ~ 5 until cleaning completed

## Easy Installation & Mobilization



Project		Customer	Oil Field / Operator	Qty
	Floating Production Unit	TOTAL	Moho Bilondo field, Congo	10 sets
	Floating Floduction Onit	AKA 100c	Bahregan field, Persian Gulf, Iran	101 sets
Offshara	Floating Storage and Offloading Unit	III SC	Abu Cluster field, Malaysia	55 sets
Offshore			Bunga Orkid field, Malaysia	46 sets
		PERO ETIMA	Bach Ho field, Vietnam	57 sets
	Floating Production Storage and Offloading Unit	Petrofac	Cendor Phaze II field, Malaysia	48 sets
Onshore			North Refineries, Iraq	44 sets
	External Floating Roof Tank	de	Al Ghaith, Qatar	1 full system
		0	Akita Oil Storage, Japan	10 sets

# Floating-Roof Tank Cleaning System

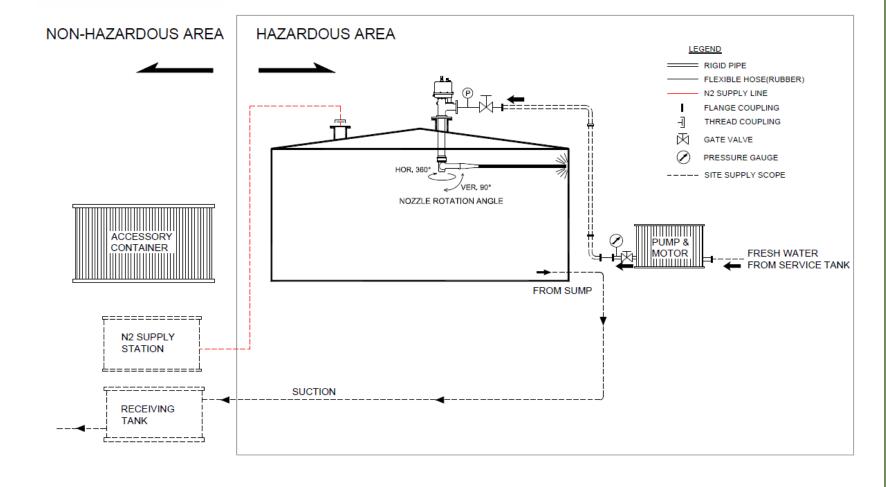


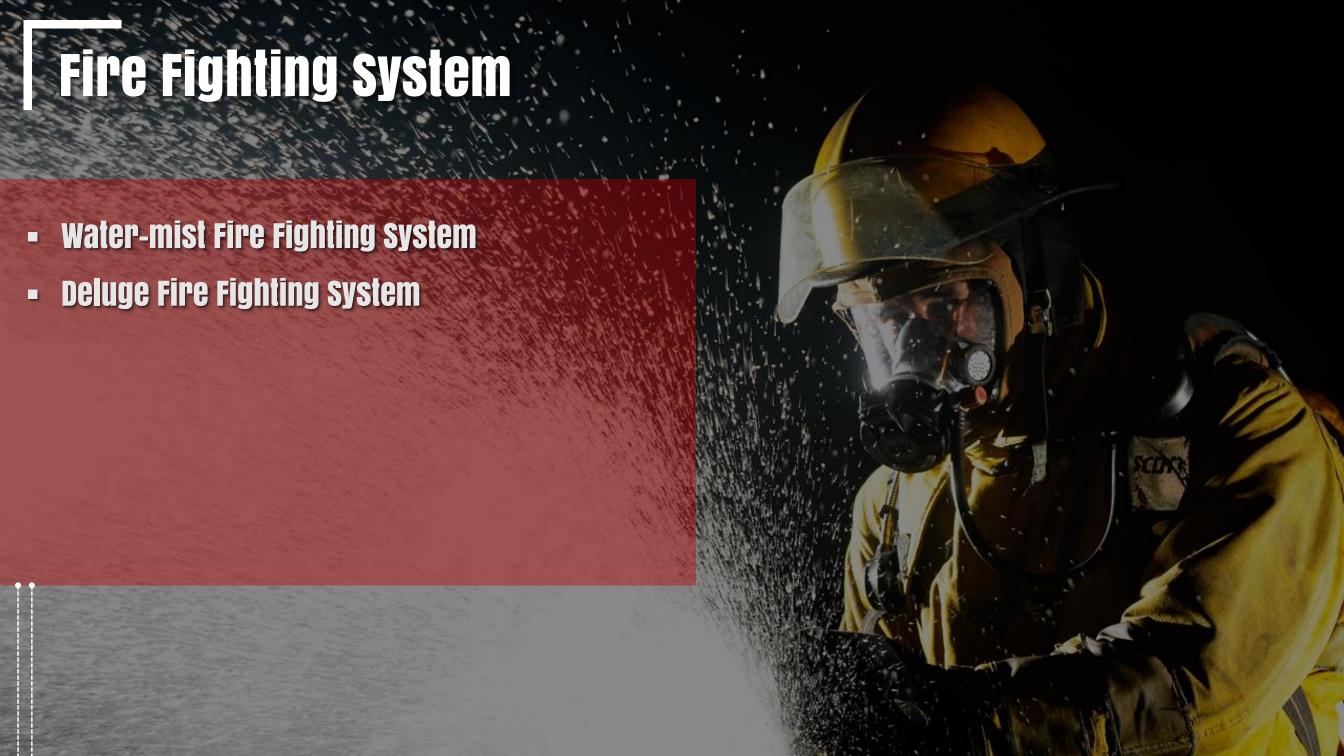
# **cone-Roof Tank Cleaning System**

## **Operation Concept**



## Schematic Drawing





## **Water-Mist Fire Fighting System**



**X-MIST® SYSTEM** is the next generation of fire fighting solutions and this system extinguishes fires by water vapor(water-mist). The exceptional cooling effect of water mist is a result of the division of water into very fine droplets, which increase the total surface area available to absorb heat and maximizes the evaporation rate of the water. All fire types, ie.A, B, C type, can be covered by this new fire fighting system.



## **System Component**

#### Pump Unit (MOV type)



#### **Main Control Panel**



Receive fire signal from alarm control panel.

Operate pump/motor and section valve. Check an error of system.

## Local Control Panel

The panel is installed at each section. Manual release of water mist.



#### Smoke / Flame Detector





#### **Alarm Control Panel**



Receive fire data from detector consisted loop.

#### Fire Monitor (Repeat Panel)



main control panel.

Display the state
of fire at each section.

## **Major Component**

#### **Water-Mist Nozzles for Local Area Application**







### **Water-Mist Nozzles for Total Flooding Application**





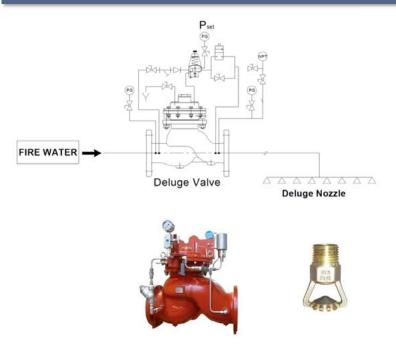
## Deluge Fire Fighting System



**Deluge system** is keeping closing state. When fire breaks out or in other emergency situation, the system is opened by electric actuating or manual and supply the fire water or foam to each deluge nozzle of the fire water line. And this system has the pressure regulating function which can preset the outlet pressure and supply the fire water as the preset pressure when the valve is opened.

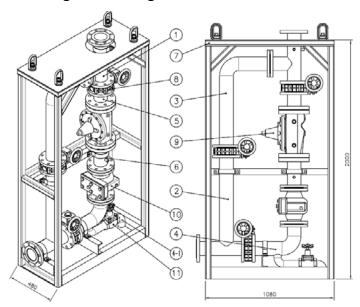


## Schematic Drawing & Major Component



## System Design Capacity

■ Deluge Full Package: Valve + Nozzle + Control + Foam + Skid





# 3

# Quality Management

**Quality Management System ERP Management System** 

# **Quality Management System**

## **QUALITY CERTIFICATION**





## **CLASS CERTIFICATION**





















# **ERP Management System**

# **ERP SYSTEM INTEGRATION TOP MANAGEMENT ERP CONTROLLER ACCOUNT PRODUCTION HUMAN RESOURCE TECH. SALES PRODCUREMENT CUSTOMER** SUB-VENDOR

## **ERP SYSTEM APPLICATION**





# 4 Major customers

**customer List** 

# **Major customers**



























قطر للبترول الدولية Qatar Petroleum International







**CPC** Corporation

**PERTAMINA** 









PETRO VIETNAM

KNPC























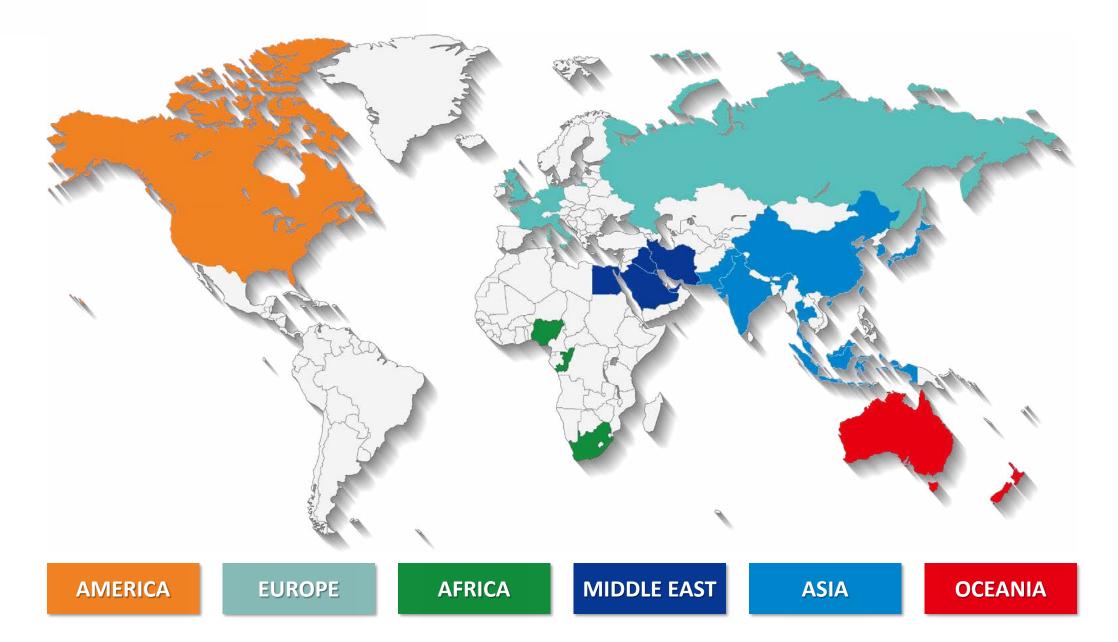




# 5 World-wide Networks

**KSPC Networks Map** 

# **KSPC Networks Map**



When was the last time you got really good safety protection?

SAFETY & PROTECTION FULL-TIME GUARANTEE

